

LECTURE 2

CONTINUED

P_T 2: T.D. OF INTERFACES

- YOUNG-LAPLACE LAW
REVISITED

- CONSIDER A SYSTEM OF
FIXED VOLUME IN THERMAL
CONTACT W/ A "HEAT
RESERVOIR", i.e. A SYSTEM
SO LARGE THAT ITS TEMP-

TEMPERATURE REMAINS CONSTANT
EVEN AFTER LARGE HEAT
TRANSFERS ΔQ .

• THEN WE HAVE: T_R (T FIXED) \circ

$$\Delta[U - TS] = \Delta U - \cancel{T} \Delta S - S \cancel{\Delta T}$$

$$= -\Delta U_R - T_R \Delta S$$

$$\left[\begin{array}{c} \text{1ST} \\ \text{LAW} \end{array} \right] \uparrow = -T_R \underbrace{\Delta S_R}_{\text{ENT. OF RESERVOIR}} - T_R \underbrace{\Delta S}_{\text{ENT. OF SYSTEM.}}$$

$$= -T_R \left[\underbrace{\Delta S_R + \Delta S}_{\text{TOTAL ENTROPY}} \right] \leq 0 \left[\begin{array}{c} \text{2ND} \\ \text{LAW} \end{array} \right]$$

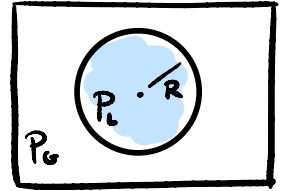
• So ANY SYSTEM UNDERGOING
A PROCESS @ FIXED VOLUME &
TEMPERATURE WILL EVOLVE TO
MINIMIZE THE "HELMHOLTZ FREE
ENERGY" $F = U - TS$

- CONSIDER A DROP OF LIQUID
IN A FIXED VOLUME OF

GAS @ FIXED TEMPERATURE:

$$dF_G = d[U_G - TS_G]$$

$$= [dU_G] - T dS_G$$



$$= [\cancel{T dS_G} - P_G dV_G - \mu_G dN_G] - \cancel{T dS_G}$$

$$= -P_G dV_G - \mu_G dN_G$$

- LIKEWISE: $dF_L = -P_L dV_L$

- AND: $dF_S = \gamma dA$

SURFACE / INTERFACE

- NOW $dV_L = -dV_G$, $dN_L = -dN_G$

$$\& \quad dV_L = 4\pi R^2 dR,$$

$$dA = 8\pi R dR$$

- so: $dF = d[F_G + F_L + F_S] = dF_G + dF_L + dF_S$
 $= -(P_L - P_G)dV_L + \gamma dA + [\mu_L - \mu_G]dN_L$

- minimizing F THEN requires:

- $\mu_L = \mu_G$

- $[P_L - P_G] 4\pi R^2 dR = \gamma 8\pi R dR$

$$\Rightarrow P_L - P_G = 2\gamma/R \quad \checkmark$$

- EULER'S THEOREM

AND SURFACE ENERGY/ENTROPY

- FOR AN EXTENSIVE FUNCTION

$Z(x, \dots, y)$ OF EXTENSIVE

VARIABLES x, \dots, y WE HAVE:

$$Z(x, \dots, y) = Z_x x + \dots + Z_y y$$

WHERE $dz = z_x dx + \dots + z_y dy$

• So :

$$u_s = TS_s + \gamma A_s$$

OR $F_s = u_s - TS_s = \gamma A_s$

OR $f_s = F_s / A_s = \gamma$

ALSO : $dF_s = \gamma dA_s - S_s dT$

• Evidently :

$$\gamma = \left. \frac{\partial F_s}{\partial A_s} \right|_T, \quad S_s = - \left. \frac{\partial F_s}{\partial T} \right|_{A_s}$$

• NOW, FOR ANY SMOOTH
Function :

$$\frac{\partial}{\partial x} \frac{\partial}{\partial y} z = \frac{\partial}{\partial y} \frac{\partial}{\partial x} z$$

- So that :

$$\left. \frac{\partial \gamma}{\partial T} \right|_{A_s} = - \left. \frac{\partial S_s}{\partial A} \right|_T = - \frac{S_s}{A} = -s_s$$

$$\Rightarrow s_s = - \left. \frac{\partial \gamma}{\partial T} \right|_{A_s}$$

- So we can measure ^{density} SURFACE ENTROPY BY MEASURING Temp DEPENDENCE OF SURF-TENS!

- SURFACE ENERGY DENSITY CAN BE MEASURED

Similarly :

$$u_s = \frac{U_s}{A_s} = \frac{F_s + TS_s}{A} = f_s + Ts_s$$

$$= \gamma - T \left. \frac{\partial \gamma}{\partial T} \right|_{A_s}$$

FROM P.I.C., sec. 3.3

Table 3.1: Surface tension, surface entropy, surface enthalpy, and internal surface energy of some liquids at 25°C.

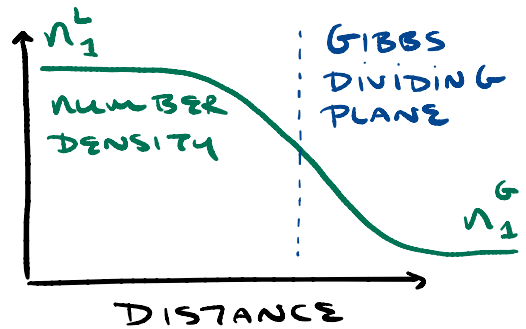
	$\gamma = f^\sigma (\text{mNm}^{-1})$	$T \cdot s^\sigma (\text{mNm}^{-1})$	$u^\sigma (\text{mNm}^{-1})$
Mercury	485.48	61.1	549.6
Water	71.99	46.9	121.1
<i>n</i> -hexane	17.89	30.5	49.9
<i>n</i> -heptane	19.65	29.2	50.3
<i>n</i> -octane	21.14	28.3	50.9
<i>n</i> -nonane	22.38	27.9	51.7
<i>n</i> -decane	23.37	27.4	52.2
Methanol	22.07	23.0	46.3
Ethanol	21.97	24.8	48.0
1-propanol	23.32	23.1	47.6
1-butanol	24.93	26.8	53.0
1-hexanol	23.81	29.8	55.6
Toluene	27.93	35.4	65.1

- GIBBS DIVIDING SURFACE
OF I.F. CHEM. OF SOLUTIONS
- WHERE IS THE INTERFACE,
PRECISELY?
- GIBBS DEFINES THE INTERFACE
TO BE A SURFACE OF
CONSTANT SOLVENT

CONCENTRATION w/ THE
PROPERTY THAT:

$$n_1^G V_1^G + n_1^L V_1^L = N_1$$

- WHERE SUBSCRIPT 1
DENOTES THE SOLVENT
SPECIES & n_1^G , n_1^L DENOTING
RESPECTIVELY THE ^{ASYMPTOTIC} NUMBER
DENSITY OF THE SOLVENT IN
THE BULK OF THE GAS &
LIQUID:



- FOR LIQUID - GAS INTERFACES
THAT ARE NOT SINGLE - COMP-
ONENT, WE MUST CONSIDER

SEVERAL CHEMICAL SPECIES

W/ TOTAL MOLE NUMBERS

N_1 , N_2, \dots, N_m .
SOLVENT SPECIES SOLUTE SPECIES

- NOW FOR $i \neq 1$ WE HAVE
IN GENERAL:

$$\underbrace{n_i^G V_i^G}_{N_i^G} + \underbrace{n_i^L V_i^L}_{N_i^L} \neq N_i$$

- THE DIFFERENCE

$$N_i - [N_i^G + N_i^L] = N_i^S \quad \text{NORMALIZED}$$

TO THE SURFACE AREA A

IS TERMED THE "SURFACE EXCESS"

$$\Gamma_i = N_i^S / A$$

• GIBBS ADSORPTION ISOTHERM

- CONSIDERING NOW A SINGLE SOLUTE SPECIES

DISSOLVED IN A SOLVENT,
WE NOW NEED TO INCLUDE

N_2^S AS A SURFACE STATE
VARIABLE ALONG WITH

ENTROPY S_s AND AREA A_s

$$dU_s = TdS_s + \gamma dA_s + \mu_2^S dN_2^S \quad (1)$$

- BUT AGAIN FROM EXTENSIVITY:

$$U_s = TS_s + \gamma A_s + \mu_2^S N_2^S$$

$\Rightarrow dU_s$ is ALSO:

$$= TdS_s + S_s dT + \gamma dA_s + A_s d\gamma + \mu_2^S dN_2^S + N_2^S d\mu_2^S \quad (2)$$

- SUBTRACTING (1) FROM (2):

$$\underline{dU_S} - \underline{dU_s} = 0$$

$$\Rightarrow S_S dT + A_S d\gamma + N_2^S d\mu_2^S = 0$$

- @ const temp: $dT \rightarrow 0$:

$$d\gamma = -\Gamma_2 d\mu_2^S$$

- WHEN INTERFACE IS IN EQUILIBRIUM w/ SOLUTION:

$$\mu_2^S = \mu_2^L = \mu_2^0 + RT \ln \frac{a}{a_0}$$

- WHERE a IS THE

ACTIVITY OF SOLUTE IN SOLUTION

[@ LOW ^{SOLUTE} CONCENTRATIONS c ,
 $a \propto c$]

$$\Rightarrow d\mu_2^S = d\mu_2^L = RT d \ln a$$

(3)
"GIBBS
ISOTHERM"

$$\left[\begin{aligned} \Gamma_2 &= -\frac{1}{RT} \frac{\partial \gamma}{\partial \ln a} \Big|_T \\ \text{OR} &= -\frac{a}{RT} \frac{\partial \gamma}{\partial a} \Big|_T \end{aligned} \right]$$

• MICELLES

- THE FOLLOWING PLOT SHOWS THE MEASURED SURFACE TENSION OF DIFFERENT

"LYSOPHOSPHOLIPIDS"

HYDROPHOBIC

W/ FATTY

ACID CHAIN

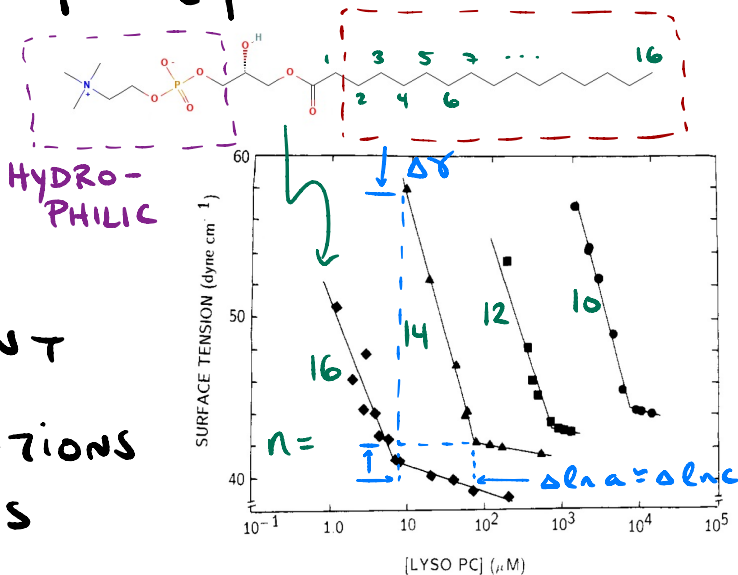
LENGTH n

@ DIFFERENT

CONCENTRATIONS

IN AQUEOUS

SOLUTION :



- SINCE THE MOLECULES HAVE A SURFACTANT-LIKE ^{HYDROPHILIC} + ^{HYDROPHOBIC} STRUCTURE, IT IS NOT SURPRISING THAT WE OBSERVE A DECREASE IN SURF. TENS. w/ INC. PHOSPHOLIPID CONCENTRATION.
- SETTING ASIDE FOR THE MOMENT THE DISCONTINUITY IN THE SLOPE @ HIGHER CONCS, WE CAN EVIDENTLY APPLY THE GIBB'S ISOTHERM TO ESTIMATE THE SURFACE EXCESS:
- TAKING THE $n = 14$ ["TETRA-DECA"] PHOSPHOLIPID DATA:

$$\bullet \Gamma_2 = - \frac{1}{2.5 \text{ kJ/mol}} \times \frac{[58 - 42] \text{ mN/m}}{[\ln 10^1 \mu\text{M} - \ln 10^{0.8} \mu\text{M}]}$$

FROM (3)

$$= + \frac{1 \text{ mol}}{2.5 \times 10^3 \text{ J}} \times \frac{16 \times 10^{-3} \text{ J/m}^2}{+0.8 \times \ln 10}$$

$$= 3.6 \times 10^{-6} \text{ mol/m}^2$$

$$= 3.6 \times 10^{-6} \times 6 \times 10^{23} \text{ molecules}$$

$$\frac{10^{20} \text{ \AA}^2}{\text{m}^2}$$

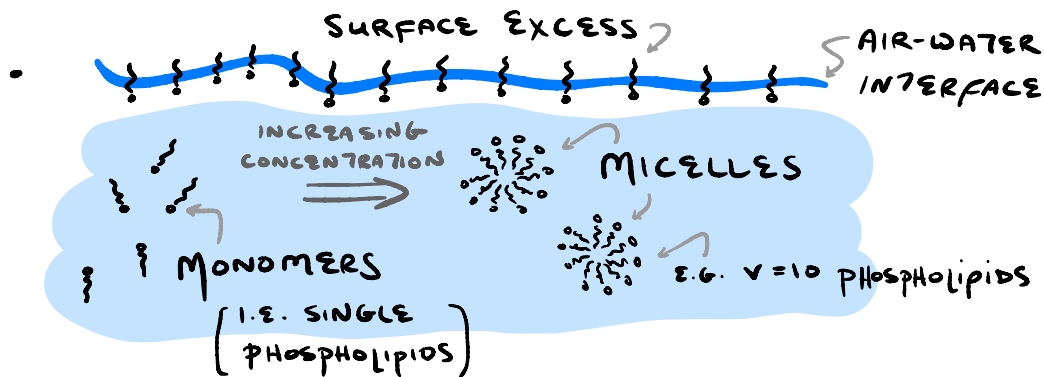
$$= 0.021 \text{ molecules / \AA}^2$$

OR :

$$50 \text{ \AA}^2 / \text{molecule}$$

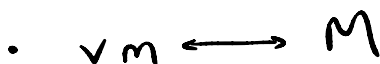
• AND WHAT ABOUT THE "KINK" IN THE SLOPE @ HIGHER CONCENTRATIONS?

• "MICELLE" FORMATION IN SOLUTION:



• **MASS ACTION:**

• CHEMICAL REACTION IN SOLUTION:



→ : "v MONOMERS CLUSTER TO FORM ONE MICELLE"

← : "ONE MICELLE DISSOCIATES INTO v MONOMERS"

• IF C & C' ARE RESP. THE CONCENTRATIONS OF MONOMERS AND MICELLES, THEN FROM LAW OF MASS ACTION WE HAVE:

$$\frac{C^v}{C'} = \exp\left[\frac{\Delta G^\circ}{RT}\right] = K \leftarrow \text{EQUILIBRIUM CONST.}$$

$$\Delta G^\circ = G_{\text{micelle}}^\circ - v G_{\text{monomer}}^\circ$$

"STANDARD GIBBS"

@ $C'=1$ @ $C=1$

IN MOLES LITER

• @ SUFFICIENTLY LOW MONOMER CONC.,

WE WILL CLEARLY HAVE NO MICELLES:

$$\lim_{C \rightarrow 0} \frac{C'}{C} < \lim_{C \rightarrow 0} \frac{C^v}{C} = \lim_{C \rightarrow 0} C^{v-1} = 0 \text{ FOR } v > 1$$

• Q WHAT CONC. DO WE START TO HAVE SIGNIFICANT MICELLE CONTENT?

• ASKED ANOTHER WAY:

• Suppose we add a small amount ϵ of monomers to solution.

• A fraction x of these

molecules will go towards formation of new micelles,

while the remaining fraction $1-x$ stay as monomers.

• x depends on the existing conc.

• E.G. we said $x \rightarrow 0$ as

$c \rightarrow 0$.

• Q WHAT CONC. DOES

$x = 50\%$?

$$\frac{c}{c'} = K = \frac{[c + \epsilon(1-x)]^v}{c' + \epsilon x / v}$$

$$\left[\text{FOR SMALL } \epsilon \right] \approx \frac{c}{c'} \times \frac{1 + \frac{v\epsilon}{c}(1-x)}{1 + \epsilon x / v c'}$$

$$\Rightarrow \frac{v}{c} (1-x) = x / \sqrt{c'}$$

$$\Rightarrow x = \left[1 + \frac{1}{\sqrt{2}} \times \frac{c}{c'} \right]^{-1} \quad (3)$$

$$\text{So IF } x = \frac{1}{2} \Rightarrow c' = \frac{c}{\sqrt{2}}$$

• SO WHEN # MONOMERS IN MICELLES
 $= \frac{1}{\sqrt{2}} \times \# \text{ MONOMERS } \phi$
 IN MICELLES.

• @ $x = \frac{1}{2}$ WE THUS HAVE:

$$\frac{c^v}{c/\sqrt{2}} = \exp\left(\frac{\Delta G^\circ}{RT}\right)$$

$$\Rightarrow RT \ln c = - \frac{2 \ln v}{v-1} RT + \frac{\Delta G^\circ}{v-1} \left\{ \begin{array}{l} \nearrow \approx \text{STD. GIBBS} \\ \text{RXN ENERGY} \\ \text{PER MOLE OF} \\ \text{MONOMER} \end{array} \right.$$

• FOR $\Delta G^\circ \gg RT$ WE NEGLECT THE
 $\ln v$ TERM.

$$\nearrow \{ \text{"CMC"} \}$$

• SO @ THE "CRITICAL MICELLE CONCENTRATION"

(5) $c_{\text{CMC}} \approx \exp\left(\frac{\Delta G^\circ}{vRT}\right)$ THE MONOMERS

BECOME UNSTABLE W/ RESPECT TO THE

FORMATION OF SMALL GLOBULAR HYDRO-PHOBIC/
 HYDROPHILIC INTERFACES, I.E. MICELLES.

- @ "TOTAL MONOMER CONC." $C + \nu C' \gg C_{CMC}$,
WE EXPECT $X \rightarrow 100\%$, SO THAT
ADDING MORE SURFACTANT WILL HAVE
NO EFFECT ON THE MONOMER CONC. C
IN SOLUTION.

- THIS EXPLAINS THE "FLATTENING" OF
THE γ VS. CONCENTRATION CURVES
SHOWN ABOVE:

- Γ IS SENSITIVE ^{ONLY} TO MONOMER CONC
 C , NOT TOTAL CONC. $C + \nu C'$.

- THERE IS STILL THE LINGERING QUESTION
OF WHY THE MONOMER \rightarrow MICELLE
TRANSITION @ $C \approx C_{CMC}$ IS APPARENTLY
DISCONTINUOUS.

- LET'S LOOK @ HOW X CHANGES FOR A
SMALL FRACTIONAL CHANGE IN CONC NEAR :
 $C = C_{CMC}$

$$\bullet C \rightarrow (1 + \alpha) C_{cmc}, \quad \alpha \ll 1$$

$$\Rightarrow C' \rightarrow \frac{C_{cmc}}{\sqrt{2}} + \alpha \frac{C_{cmc}}{\sqrt{2}} = \frac{C_{cmc}}{\sqrt{2}} [1 + \sqrt{2} \alpha]$$

$$\text{WHY?} \bullet @ \alpha \rightarrow 0 \quad C = C_{cmc}$$

$$\Rightarrow x = \frac{1}{2}$$

$$\Rightarrow C' = \frac{C}{\sqrt{2}} = \frac{C_{cmc}}{\sqrt{2}}$$

• SINCE $x \approx \frac{1}{2}$, AN INCREASE ΔC

IN C IMPLIES AN INCREASE $\Delta C' = \frac{\Delta C}{\sqrt{2}}$

FROM

IN C' .

(4):

$$\bullet x = \frac{1}{2} + \Delta x = \left[1 + \frac{(1 + \alpha) C_{cmc}}{\sqrt{2} \frac{C_{cmc}}{\sqrt{2}} (1 + \sqrt{2} \alpha)} \right]^{-1}$$

$$\text{FOR } \alpha \ll 1: \approx \left[1 + (1 + \alpha)(1 - \sqrt{2} \alpha) \right]^{-1}$$

$$\approx \left[2 \left(1 - \left(\frac{\sqrt{2}-1}{2} \right) \alpha \right) \right]^{-1}$$

$$\approx \frac{1}{2} \left[1 + \left(\frac{\sqrt{2}-1}{2} \right) \alpha \right]$$

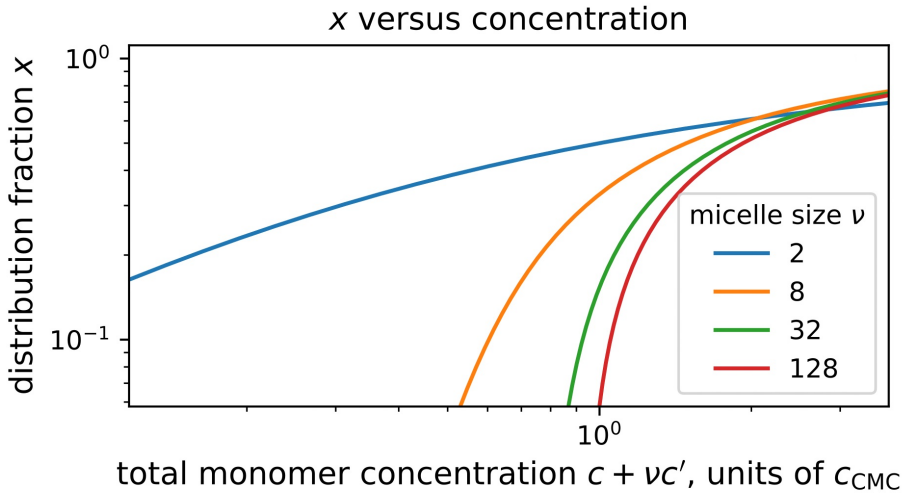
$$\Rightarrow \left. \frac{dx}{d\alpha} \right|_{C=C_{cmc}} = \frac{1}{4} \left(\frac{\sqrt{2}-1}{2} \right)$$

1.2. $\frac{\sqrt{2}}{2}$

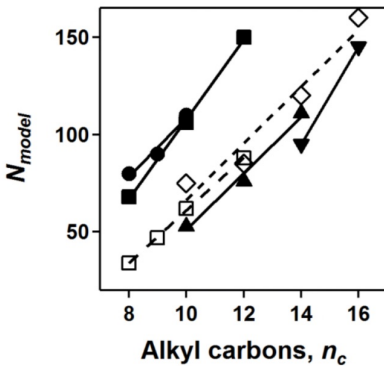
• SO: THE BIGGER THE MICELLE, THE

THE FASTER THE TRANSITION $x = 0\% \rightarrow 100\%$!

- A MORE COMPLETE NUMERICAL SOLUTION OF THE MODEL GIVES:



- TYPICAL MICELLE SIZES ARE QUITE LARGE : $v \approx 50 - 150$:



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HERE IS A PLOT OF "MONOMER NUMBER" [WHAT WE CALL v] AS ESTIMATED FROM X-RAY SCATTERING FOR DIFF. DETERGENT MONOMERS VS. HYDROPHOBIC TAIL LENGTH n_c . SEE CITED ARTICLE FOR DETAILS.

* IS THE $N_c = v \propto n_c$ CORRELATION IN LINE W/ YOUR EXPECTATIONS?